

RESEARCH ARTICLE

Methane removal using materials from biofilters at composting plants

Loại bỏ khí Mê-tan bằng cách sử dụng vật liệu trong các bể lọc khí sinh học ở các cơ sở sản xuất phân vi sinh

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Methane (CH₄) source of Greenhouse Gases should be considered; CH₄ is formed by composting under anaerobic conditions. Using microbial Methane oxidation is a solution with low cost and effective. In this study, 27 bio-filters and 18 laboratory-scale bioreactors were used to investigate the potential for CH₄ removal in biogas. The CH₄, Dinitrogen monoxide (N₂O) and Carbon dioxide (CO₂) concentrations at the inlet and outlet of the air purifier were measured by gas chromatography. The results showed that the CH₄ concentration decreased in experiments while the CO₂ and N₂O content increased in all experiments. An experiment was conducted with 1 kg of biofilter material with the input of 800 ppm CH₄ contained in a 5-liter flask for 49 hours containing. The results also showed that the CH₄ concentration decreased by 71% after 20 hours and N₂O was formed in the reactor.

Mê-tan (CH₄) là nguồn khí gây nên hiệu ứng nhà kính cần được quan tâm, khí CH₄ được sinh ra trong quá trình ủ vi sinh trong điều kiện kị khí. Một giải pháp với chi phí thấp là sử dụng vi sinh vật oxy hóa khí CH₄ cố định trên giá thể là vật liệu sử dụng trong thiết bị lọc sinh học. Trong nghiên cứu này, 27 thiết bị lọc sinh học trên thực tế và 19 bình lọc tại phòng thí nghiệm đã được sử dụng nhằm mục đích khảo sát khả năng loại bỏ CH₄ có trong khí sinh học. Nồng độ khí CH₄, N₂O và CO₂ ở đầu vào và đầu ra bể lọc khí được đo đạc bằng phương pháp sắc ký khí. Kết quả cho thấy nồng độ khí CH₄ giảm sau khi qua hệ thống lọc sinh học ở một số bình, trong khi nồng độ khí CO₂ và N₂O lại tăng lên ở tất cả các bình. Khi khảo sát khả năng oxi hóa CH₄ ở nồng độ 800 ppm của 1kg vật liệu thiết bị lọc sinh học chứa trong bình phản ứng thể tích 5L với thời gian 49 giờ. Kết quả cho thấy nồng độ.

Keywords: greenhouse gas, emissions, composting, windrows, organic waste, methane, biofilter

1. Introduction

Methane (CH₄) and Dinitrogen monoxide (N₂O) are considered to be strong Greenhouse Gases (GHGs), whereas NH₃ is identified as an odour component and an indirect GHG. According to the Intergovernmental Panel on Climate Change (henceforth IPCC) Report in 2007, the Global Warming Potential (GWP) of CH₄ and N₂O in100 years are respectively 25 and 298 times higher than that of CO₂. CH₄ emissions from livestock account for 37% of the total emissions of CH₄ in global, mainly for ruminants in digestion. In addition, landfill gas collection has been established to generate electricity and heat in many countries. The CH₄ emitted from landfills is one of the major sources accounting for approximately 30% of total CH₄ emissions (Kára et al., 2010). In other cases, flares are operated to burn CH₄ and other organic trace compounds contained in the landfill gas before releasing to the atmosphere. However, these

processes cannot be applied in cases of low CH_4 concentration. Up to now, the mitigation of emissions with low CH_4 concentrations often is neglected.

 CH_4 removal was observed with low gas flows and high concentrations in the soil or in biofilters (Bender & Conrad, 1992). In a biofilter, an autochthonous methanotrophic biofilm can develop and use CH_4 as a carbon source. However, the CH_4 removal in biofilters varied from case to case due to different working conditions e.g. ambient temperature, humidity and nutrient content.

Most of the previous reports (Scheutz *et al.*, 2009; Melse & Van De Werf, 2005 and Bender & Conrad, 1992) showed that a good CH₄ oxidation rates of 20% CH₄ in the supply air and 2.5% CH₄ in the exhaust air. Biofilter has a high flow rate in a combination of low concentrations of CH₄. Low CH₄ concentrations range of below 0.07% CH₄ (700 ppm \sim 460 mg CH₄/m³) in combination with a high exhaust air volume flow in the range of 20,000 - 50,000 m³/h. This results

in a biofilter had a load of about 100 m³/m³.h. The efficiencies of CH₄ reduction range from 0% - 20% (Scheutz *et al.,* 2009). In addition, Melse and Van De Werf (2005) reported a CH₄ reduction of 80% in the biofilter with a load of 0.75 m³/m³.h.

 CH_4 oxidation is therefore considered as an important method to CH_4 emissions reduction. At present, only a few scientific publications on biological waste air treatment are available. Studies related to test the CH_4 removal capacity of a new material have not yet been done. Looking into the real conditions of the biofilter, among different microorganism, CH_4 oxidation bacteria needs to be found. Then, they will be enriched populations, which are added to the biofilter or bioscrubber on demand.

The aim of this work was to investigate CH_4 removal in different biofilters and to develop a new method to find materials for CH_4 oxidation.

2. Materials and methods

2.1 Screening of biofilters

Twenty-seven biofilters in composting plants in Germany were investigated in the study. The study was carried out from 2012 to 2014. An overview of a capsulated biofilter is shown in Figure 1. The gas before and after biofilter was analysed at each plant. At capsuled biofilters, the treated air left the biofilter in a chimney. Here the gases were measured. At the open biofilter of $16m^2$ (4x4m) was covered by a thin foil. Concentrations of the treated gases were measured under the foil.

Exhaust gases were sampled manually by evacuated head-space vials and subsequently analysed for CH₄, CO₂ and N₂O by gas chromatography (ECD/FID, SRI 8610C, USA) in the laboratory in Bonn University, Germany. It was assumed that the volumes of treated and untreated air were the same.





2.2 Experimental setup

After screening of 27 biofilters, solid samples of the biofilters' from the most CH_4 reduction was taken for laboratory experiments. The experiments were carried out in 18 batch reactors (5L) (Figure 2). Each batch reactor contained 1kg biofilter's material at the outset of the experiment (Figure 3). It was assumed that methanotrophic bacteria was available on the material. CH_4 (800 ppm) was mixed with air, humidified and introduced in the 5L reactor. The mixing was pumped into reactors for 5 minutes to push out the existing air in the reactor. After pumping, the reactor was closed and no more Oxygen (O₂) was supplied. The air in the reactor is assumed to contain ~20% O₂ together with the 800ppm CH₄. Samplings of incubated gases were taken to measure the concentrations of CH₄ and O₂.

The gases in the reactor were sampled at intervals of 1, 2, 19, 22, 24, 26 and 49 hours, and analysed for CH_4 , CO_2 and N_2O in the laboratory by GC-FID/ECD.



Figure 2. Test kit for determination of CH₄ removal capacity



Figure 3. Material of biofilter for the testing of CH_4 removal capacity

The removal performance was determined by mass balance according to the following equation:

$$CH_4 ox_i = \frac{(flux_{in} - flux_{out})}{flux_{in}} \times 100$$

With

 $CH_4 ox_i$: At the time *i* oxidized portion of inlet flow [%] Flux_{*in*}: CH₄ concentration flow into the reactor at time *i* (*i*= 1, 2, 19, 22, 24, 26 and 49 hours)

 $Flux_{out}$: CH₄ concentration flow out the reactor at time *i* (*i*= 1, 2, 19, 22, 24, 26 and 49 hours)

3. Results and discussion

3.1 CH₄ removal from biofilters at composting plants

The inlet concentration of CH_4 and CH_4 reduction of biofilters were shown in Figure 4. CH_4 was reduced and produced in the biofilters. The removal efficiency ranged from production of -260% to reduction of 80% for CH_4 . The mean concentration of CH_4 before biofilter was (106 ± 73) ppm. The average CH_4 removal efficiency was 25% at 13 biofilters. With regard to other literature, CH_4 was reduced by 15% (Amlinger *et al.*, 2008). As waste gas permeates the biofilter layer, CH_4 is oxidized to CO_2 and H_2O by methanotrophic bacteria present in the biofilter's material. The effect on the production of CH_4 emissions in the biofilter may be explained by anaerobic degradation of organic substances in the biofilter (Nguyen & Cuhls, 2016). However, it is not yet well understood.



Figure 4. Inlet CH_4 concentrations and removal efficiencies of CH_4 at the studies biofilters

Reference	CH₄ removal (%)	CH₄ removal rate max (g/m².day)
This study	7 to 27	5-56
Amlinger <i>et al.,</i> 2008	15	-
Trimborn <i>, et al.,</i> 2003	up to 26	-
Du Plessis <i>et al.,</i> 2003	-	87
Wilshusen <i>et al.,</i> 2004	-	96-276
Streese & Stegmann,	-	341
2003		
Melse & Van De Werf,	-	377
2005		
Park <i>et al.,</i> 2005	-	435
Sly <i>et al.,</i> 1993	-	586
Haubrichs & Widmann,	-	592
2006		
Note: "" mogne data was not available		

Table 1. Comparison of removal efficiency of biofilters: this study and data from literature (Scheutz *et al.*, 2009)

The reductions of CH_4 were lower than in previous studies (Table 1). Melse and Van De Werf (2005) reported the CH_4 reduction of 80% in a biofilter with the load of 0.75 m³/m³.h. However, this loading factor is 130 times lower than in practice. Previous studies illustrated that the process-controlling factors of the CH_4 oxidation in low-concentrations are the O_2 availability, storage density and gas permeability as well as the volume flow of the gas to be treated (Bender & Conrad, 1992: Benstead & King 1997 and Dunfield *et al.*, 1999). In fact, the low CH_4 removal efficiency in practice could be explained by exposure time due to a short duration of the waste air treatment in biofilters.

3.2 Methane oxidation reaction

3.2.1 The value of pH

The pH of biofilter's material was from neutral to a light alkaline (ranged from 7.16 to 7.82). The pH values were suitable for methanotrophic activities. The CH_4 removal process was observed in a broad pH range, from pH< 4 in a sand soil to pH> 9 in a bog soil. The optimal pH for methanotrophs growth is between 6 and 8 (Cao & Staszewska, 2011).

3.2.2 Methane removal and carbon dioxide generation

 CH_4 removal and CO_2 generation were investigated for the biofilter's materials. The observed decrease in CH_4 concentration in Figure 5 and 6 can be explained by oxidation since O_2 was available and CO_2 was increased. After an incubation for 49 h at 25°C, 99% of CH_4 was consumed. The CH_4 removal rate increased when the O_2 concentrations increased from 2.5% to 15% (Cao & Staszewska, 2011).

By comparison, the CH_4 concentration in the reactor was 200 ppm after 20 hours (500 ppm reduction); whereas, the CO_2 concentration was 3000 ppm (2500 ppm generation). This could be explained by aerobic decomposition of material in the reactor due to the availability of O_2 . Maximum CH_4 consumption and maximum CO_2 generation were observed at the first phase of incubation. Previous studies have shown that the rate of CH_4 removal grows with the increase of CH_4 concentration. The increase of CH_4 concentrations from 2 to 16 % leaded to 1.1 - 2.5 folds increase of the methanotrophic activity (Pawłowska & Stępniewski, 2004). Another author found that a value (2.3-folds) in the methanotrophic activity increase was observed, where the measured CH_4 concentration varied from 25 to 200 ppm (Whalen & Reeburgh, 1996).



Figure 5. \mbox{CH}_4 concentrations in the reactors during incubation time

 CO_2 concentration was increased steadily (Figure 6). CO_2 generation was increased 15 times after 49 hours of incubation (from 3,400 ppm to 57,000 ppm). Although the amounts of CH₄ removal by 3 replications were similar and decreased slightly after 20 hours' incubation, CO_2 generation increased sharply. O_2 is a significant factor influencing the CH₄ oxidation process (Cao & Staszewska, 2011).



Figure 6. $\ensuremath{\text{CO}_2}$ concentrations in the reactors during incubation time

3.2.3 Nitrous oxide formation

 N_2O generations were low at the start of the experiment and increased steadily to a maximum rate (Figure 7). The increase in N_2O concentrations during the experiment is attributed to the nitrification process.

The formation of N₂O during the further duration of the experiment indicates that some N₂O production occurred in the biofilter material. The increase of N₂O may be explained by the fact that N is converted to N₂O by nitrification due to continuous aerobic conditions in the biofilters (Melse & Van der Werf, 2005). According to previous studies, around one third NH₃ that enters biofilters can be transformed and released as N₂O (Trimborn, 2003). Similarly, Clemens and Cuhls (2003) reported that 26% of NH₃ was transformed into N₂O in biofilters.

The total cumulative N₂O generation after 50h incubation was 1.4 ppm was much lower than the reduction of CH_4 (823 ppm). After the end of the experiment, the contribution of N₂O to the total GHG concentration in the outlet air is insignificant.



Figure 7. N_2O concentrations in the reactors during incubation time

4. Conclusions

Biofilter has the capacity of CH_4 removal and reduction. This is an attractive option for CH_4 removal at low concentration in the organic waste treatment plants.

Results from experiments using biofilter's material showed that the material was an excellent property as a carrier for CH_4 oxidation processes. Application of the microbial oxidation is a promising way to control the CH_4 emission from organic waste treatment.

 CH_4 reduction rates in some biofilters were significantly lower than other. In biofilters, CH_4 is either oxidized or produced due to the O₂ availability. The CH_4 oxidation rate was lower in some part of biofilters because of the anaerobic condition. Therefore, the designing the biofilters correspondingly should effectively promote the microbial CH_4 removal of exhausted gas.

Further study is needed to understand and explain the CH_4 formation and removal in the biofilter in order to optimize the CH_4 and N_2O reduction processes. More studies with the continues reactor should be carried out because GHG emission of N_2O in the outlet air of the batch reactor was 3 times higher than the inlet gases. If it is the same tendency in the continuous reactor, it will be concerned more when the concentration of CH_4 (GPW =25) decreases 15 times when that of N_2O (GPW = 298) increases three times in biofilter.

5. References

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